

Claim 4, line 1, delete "claims 1-3" and insert

--claim 1--;

Claim 5, line 1, delete "claims 1-4" and insert

--claim 1--;

Claim 6, line 1, delete "claims 1-5" and insert

--claim 1--;

Claim 7, line 1, delete "claims 1-6" and insert

--claim 1--;

Claim 8, line 1, delete "claims 1-7" and insert

--claim 1--;

Claim 9, line 1, delete "claims 1-8" and insert

--claim 1--;

Claim 10, line 1, delete "claims 1-9" and insert

--claim 1--;

Claim 11, line 1, delete "claims 1-10" and insert

--claim 1--;

Claim 12, line 1, delete "claims 1-11" and insert

--claim 1--;

Claim 13, line 1, delete "claims 1-12" and insert

--claim 1--;

Claim 14, line 1, delete "claims 1-13" and insert

--claim 1--;

Claim 15, line 1, delete "claims 1-14" and insert

--claim 1--; and

Claim 16, line 4, delete "claims 1-15" and insert

--claim 1--.

Please add the following new claim 17:

1 17. Process according to claim 2, wherein:

2 the degree of dispersion is increased after the
3 regeneration;

4 the acid impregnated catalyst is reduced in a flow of
5 hydrogen gas;

6 the acid impregnated catalyst is oxidised in a flow of dry
7 (<0.1 vol.% of water) air, followed by reduction;

8 the reduction and or oxidising step are carried out at a
9 temperature of between 250 and 600°C;

10 the silica-alumina support has been prepared using a sol-
11 gel method;

12 the support has an Si-Al atomic ratio of from 0.1 to 300;

13 the catalyst has a precious metal content of from 0.01 to 5
14 wt.%, calculated on the basis of the weight of reduced catalyst;

15 the catalyst is impregnated with an aqueous solution of the
16 acid;

17 the acid is selected from the group of HCl, H₃PO₄, H₂SO₄

18 HNO₃, HBr and combinations thereof;

19 the amount of acid calculated on the basis of a ratio of
20 equivalents of acid to atoms of precious metal is between 0.1
21 and 100, preferably between 0.5 and 10;

22 prior to the impregnation, carbonaceous deposits on the
23 catalyst are burned off;

24 the regeneration is carried out in a reactor, separate from
25 the reactor in which the catalyst is used; and

26 the catalyst is a used catalyst from a process in the group
27 consisting of hydrogenation, hydro-isomerisation, hydro-
28 desulphurisation, hydrodewaxing and catalytic reforming.

21 18. Process for hydrogenation, hydro-isomerisation, hydro-
2 desulphurisation or hydrodewaxing, comprising treating the
3 feedstock in the presence of a catalyst that has been
4 regenerated using the process of claim 17.

REMARKS

This Preliminary Amendment puts the claims into proper form for examination. Kindly calculate the filing fee based on the amended claims.